

# Integration of Particle/Powder Technology in the ChE Curriculum

## Demonstrations and Teaching Modules



ASEE Chemical Engineering Division



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# Integration of Particle/Powder Technology Demonstrations and Teaching Modules

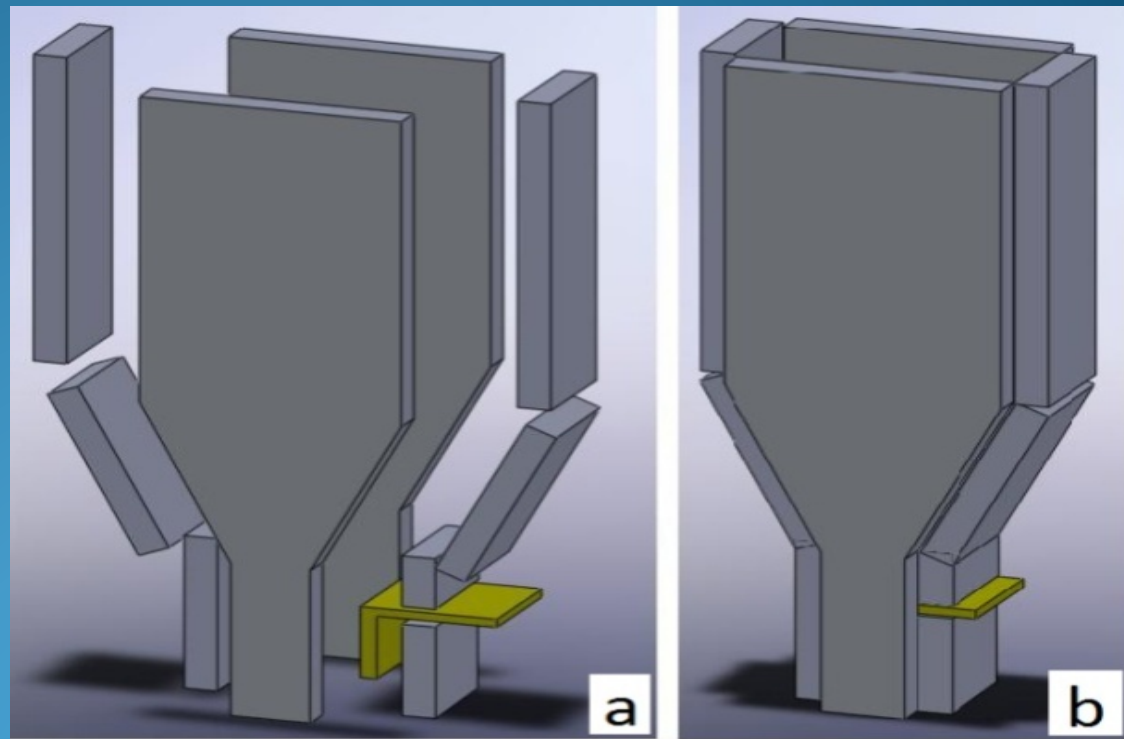
- Introduce and familiarize students with technology and industrial applications - Focus: Pharmaceutical industry
- Measurements and Analysis
  - Conductivity measurements
  - Colorimetric measurements
  - Experimental design
  - Engineering statistics (*I err therefore I am. St. Augustine*)
- Study of unfamiliar technology opens minds to new analysis techniques

# Agenda

- **Hopper flow** (video 1)
  - *Rise of large particles in bed of smaller particles*
  - **Particle mixing/segregation**
- 
- **Pneumatic conveying**
  - *Video 2*
- **V-mixing**
    - *Concept*
    - *V-mixer design and construction (detailed instructions in pdf file provided)*
    - *Experimental design and group experiment*
- **Group Formation: pick number and join group**
- **References in Excel<sup>©</sup> file provided**
  - **Additional information and tabular design format(Excel<sup>®</sup> ready) also provided**

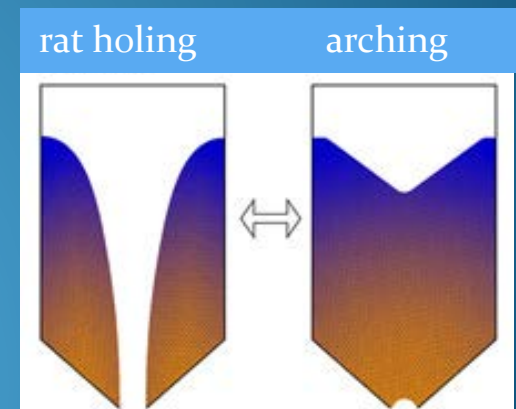
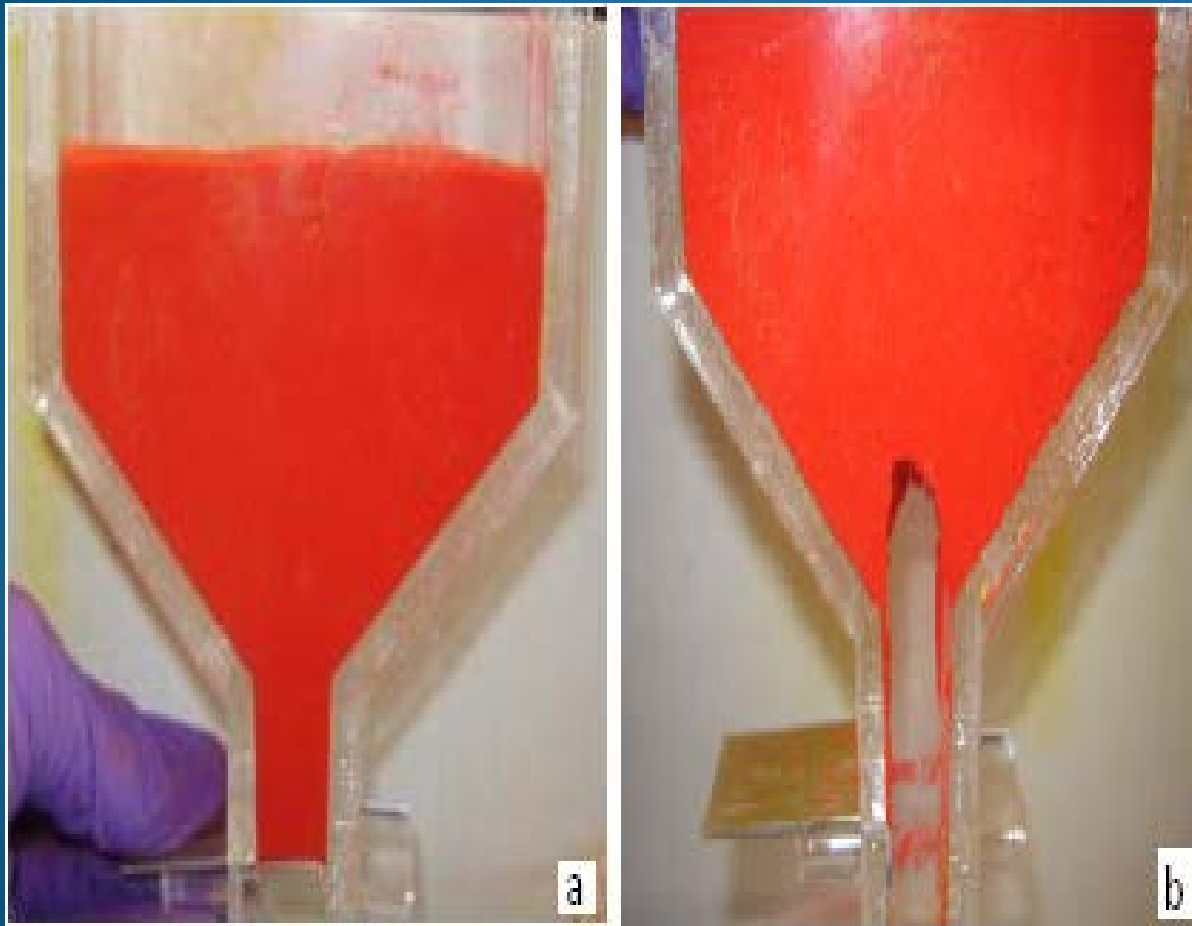
# Hopper Flow

- 2-D hopper
  - 1/4 in. clear polycarbonate, acrylic
  - brass hopper (18 gauge) “flow controller”
  - Angle: 40° and 60°
  - Acrylic bonding adhesive
  - H = 7.75”, Max. width of 5”



Hopper: (a) Un-assembled (b) Fully assembled

# Hopper Flow



$$ff = \frac{\sigma_c}{\sigma_D}$$

# Hopper Flow Factors

$$ff = \frac{\sigma_c}{\sigma_D}$$

$\sigma_c$  = hopper compacting stress

$\sigma_D$  = stress developed in powder

$\sigma_y = f(\sigma_c)$  unconfined yield stress of powder (arch surface)

Probability of arching decreases with flow factor

$$\sigma_D > \sigma_y \text{ for flow}$$

$$\frac{\sigma_c}{ff} > \sigma_y$$

- Arching function of material, temperature, moisture, corrosion and abrasion



# Hopper Flow

- <http://www.jenike.com/Solutions/poorflow.html>

video 1

# Particle Mixing/Segregation



- Clear plastic
- Hand-crank or motor

1	tumbler; $d_{\text{inner}} = 5.75"$ , length = 12"
2	gaskets $d_{\text{inner}} = 6"$
6	2" long 3/8" bolts
6	3/8" hex nuts
1	wooden base with tumbler supports



# Particle Segregation



Particles forced toward wall.  
Larger particles travel further and smaller particles “fill” spaces among larger particles

Can connect to trajectory seg./percolation

Stoke's Law distance,  $D$

$$D = \frac{U \rho_p x^2}{18\mu}$$

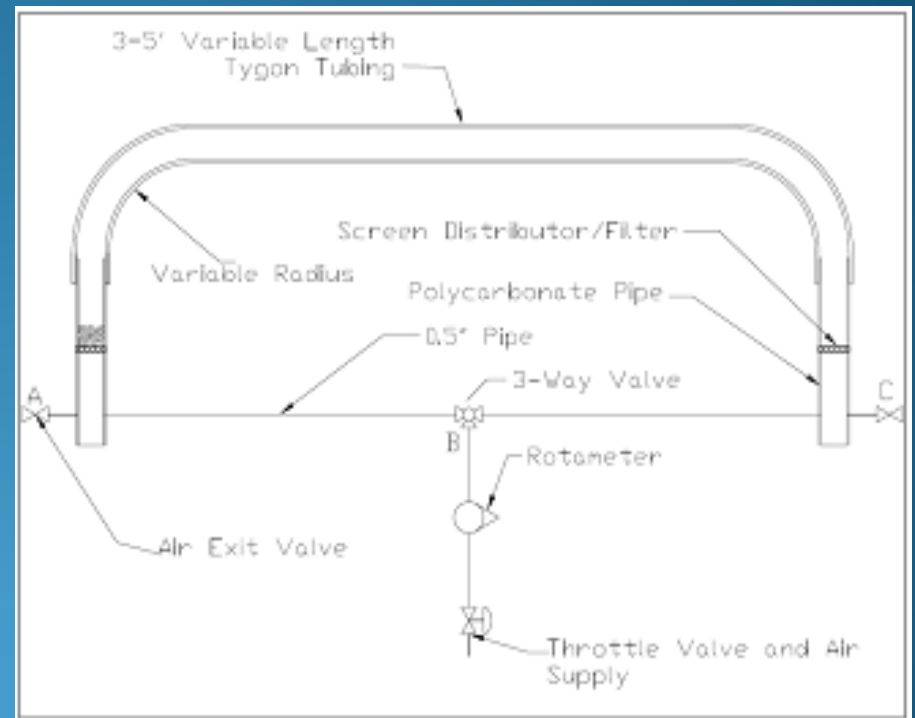
$U$  = velocity

$\rho_p$  = particle density

$x$  = particle diameter

$\mu$  = fluid viscosity

# Pneumatic Transport Apparatus (small)

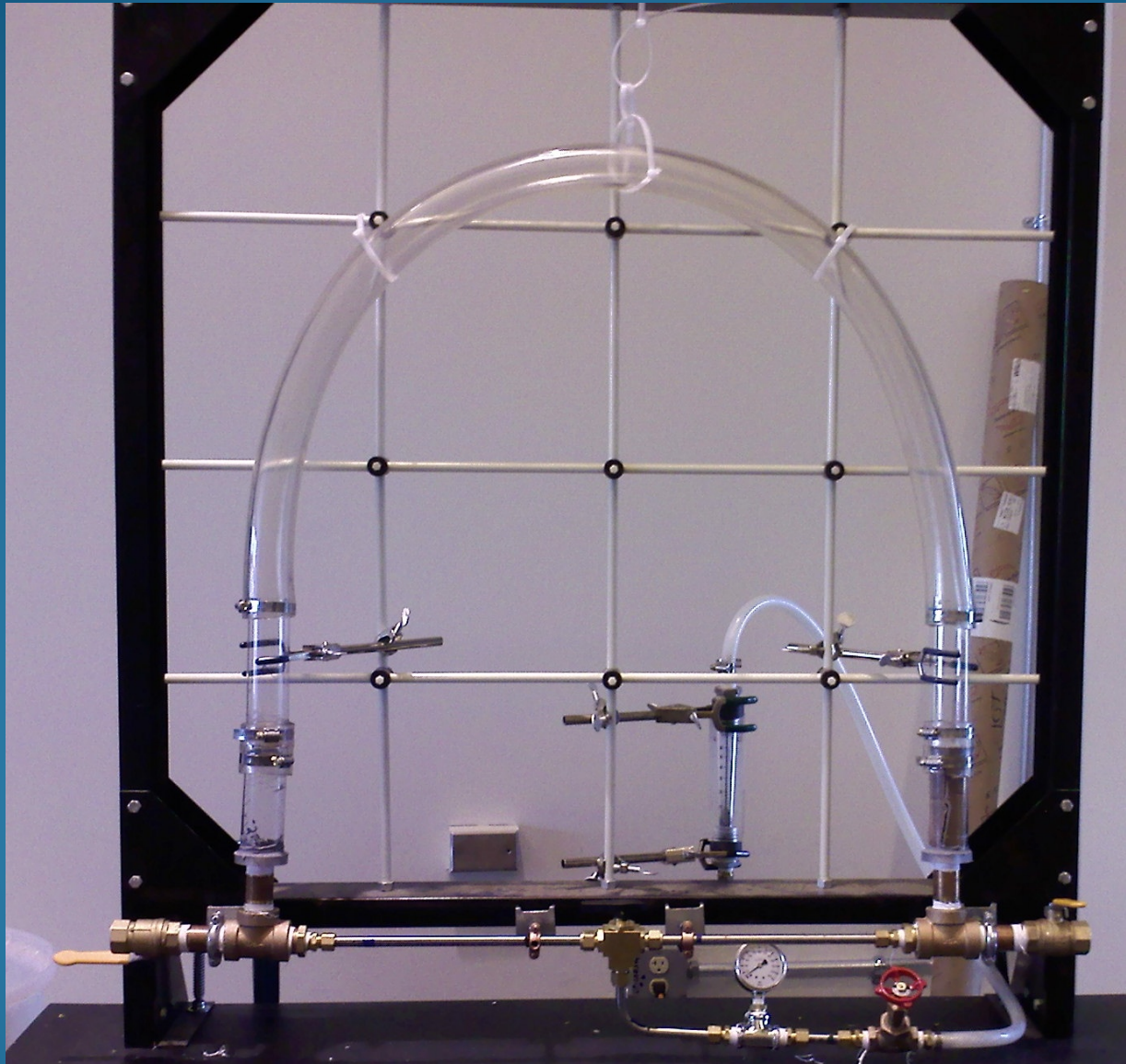


# Pneumatic Transport Apparatus Parts List (small)

<b>Part Inventory - Pneumatic Transport Apparatus - SMALL</b>			
<b>ITEM</b>	<b>QTY.</b>	<b>Specification</b>	<b>Purpose/Description</b>
1	6'	1" ID	Tygon Tubing - Thick walled
2	2'	1" OD	Polycarbonate Round tube Clear
3	2	1/2"	Threaded
4	4	1/2" X 3"	Threaded Nipples
5	1	0 - 40 SCFM	Flow meter
6	1	1/2"	Brass Ball Valve
7	6'	1/2" ID	Braided Hose Air Feed
8	1	1/2" Tube	Diverting 3 Port brass ball valve Yor Lock Fittings, Ultra High Pressure
9	5	1/2"	Brass Compression Fitting Adapter for 1/2" Tube
10	1	1/2"	Bronze Globe Valve 1" NPT Female Connections



# Pneumatic Transport Apparatus (large) – Ear Protection Required



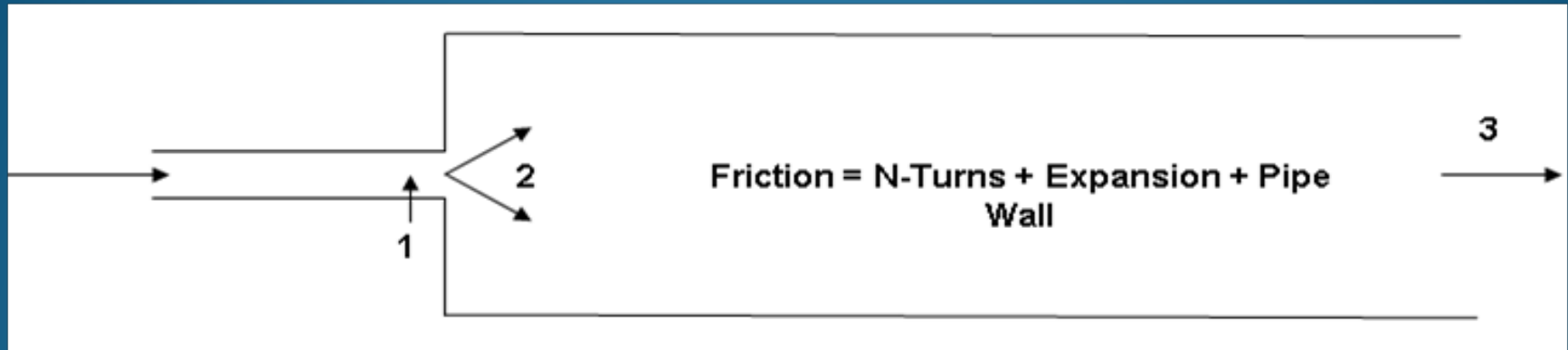
# Pneumatic Transport Apparatus Parts List (large)

## Part Inventory For Pneumatic Transport Apparatus - LARGE

ITEM	QTY.	SPECIFATION	DESCRIPTION
1	6 ft	2" ID - 2.5" OD	Tygon PVC Tubing (0.25" wall)
2	2 ft	1.75" OD 1.5" ID	Poly-Carbonate Round Tube (clear - 0.125" wall)
3	2	1.0" NPT	Brass Ball Valve - Female Connections
4	2	1.0"	Medium-Pressure Cast Brass Threaded Pipe Fitting, TEE
5	2	1" Male X 1/2" Female	Medium-Pressure Cast Brass Threaded Pipe Fitting, Hex Bushing
6	400	0.125" DIA.	Nylon Spheres
7	4	0.5" NPTF	Std. Brass Compression Tube Fitting Adapter Male Pipe
8	1	0.5" TUBE OD	Brass Ball Valve w/ YOR-LOK Fittings Diverting 3-port Ultra High Pressure
9	6" x 6"	0.125" spacing	Std. Screen/Mesh Air Distributor
10	1	1/2" class 150	Bronze Globe Valve 1" NPT Female - Throttling Valve
11	N/A	0.5" TUBE OD	Unspecified length TO BE DETERMINED
12	4	1"	Thick-wall Brass Threaded Pipe Nipple, Sch 80, 11/16" Thread Length
13	1	10-60 SCFM @ STP	Rotameter/Flowmeter

# Pneumatic Transport

## Energy Balance/Continuity



$$v_2 = \left[ \frac{(P_1 - P_2)(2RT)}{MW_{AIR}} \right]^{0.5} = \left[ \frac{\left( \frac{kgm}{s^2 m^2} \right) \left( \frac{kgm^4}{s^2 m^2 kmolK} \frac{Kkmol}{kg} \right)}{\left[ \left( \frac{D_2}{D_1} \right)^2 \left( \frac{P_2}{P_1} \right)^2 (P_1) (K_{EXPANSION} - 1) + P_2 \right]} \right]^{0.5} = \frac{m}{s}$$

Poor estimations – why?

What energy losses are not included in analysis?

Can also do minimum fluidization velocity measurements (one side –fluidized bed)

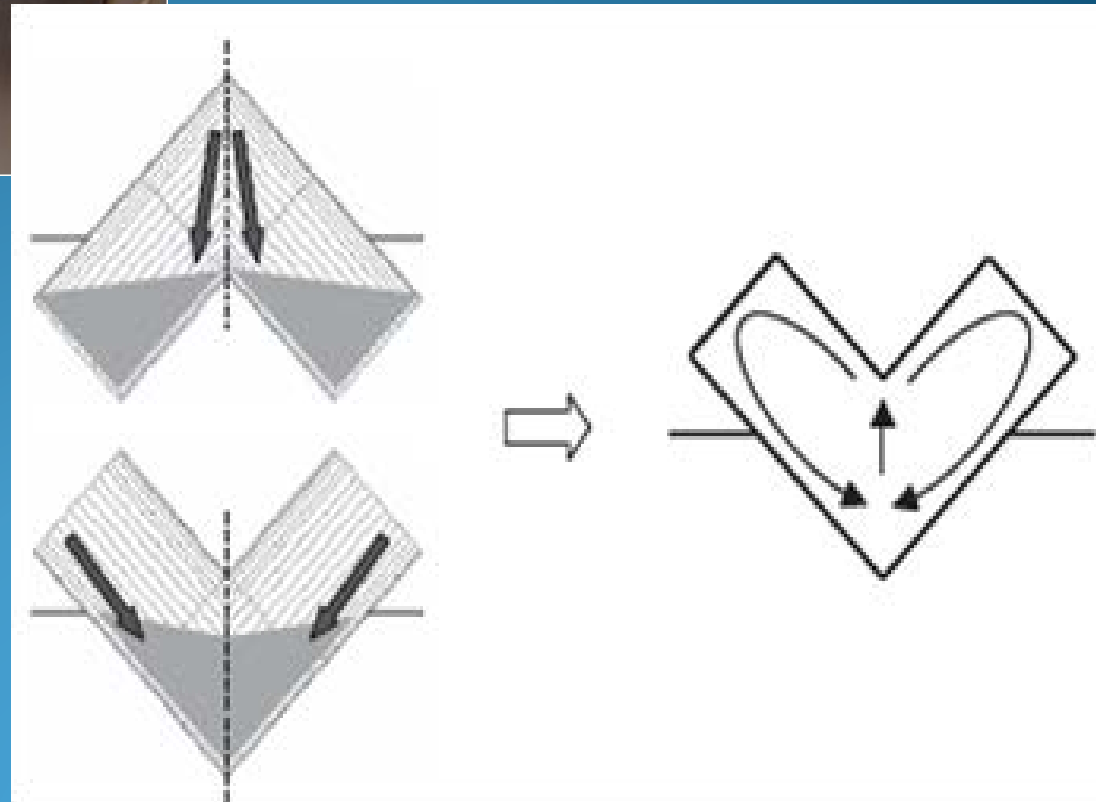
(Video 2)





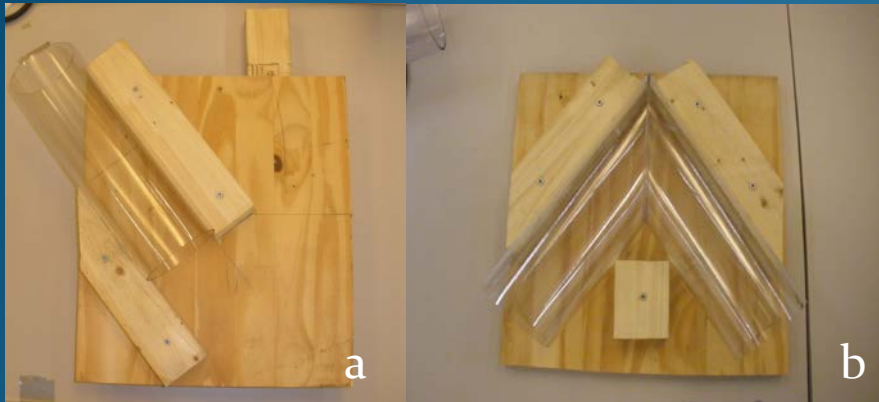
# V-Mixing

5 L constant speed V-mixer -  
[www.tabletpress.net](http://www.tabletpress.net)  
\$1650 – bench top model with timer switch  
Loading capacity – 1 kg

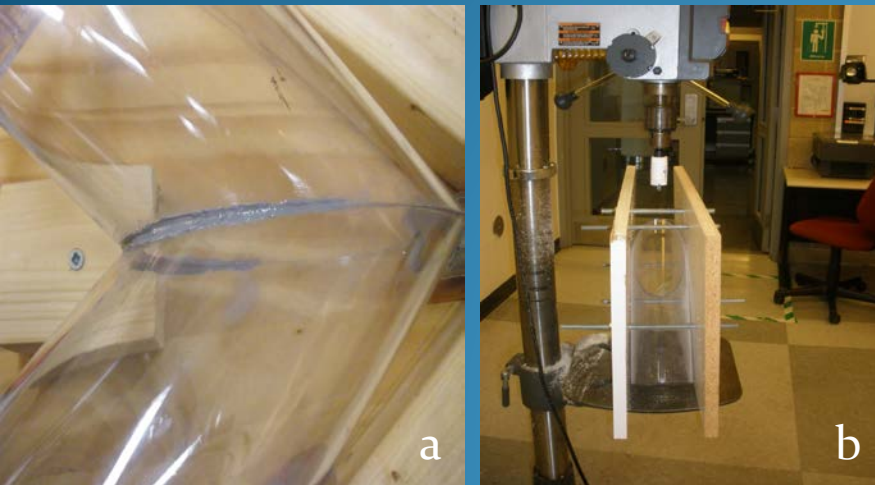


# V-Mixer Construction

(Detailed instructions in pdf file provided)



Cutting (a) and gluing tubes (b)



Epoxy (a) and drilling hole (b)



V-Mixer



Pneumatic motor

Gast Mfg. Corp (Vendor – McMaster-Carr

Model #2AM-FCW-13 with Boston gear/speed reducer 713-60-j

\$500.00

# V-mixer Demonstration

## highly visual and colorful

k-12 – engaging, ask for predictions

undergraduates – predictions based on physics, sampling, mixing quality measures, loading procedures



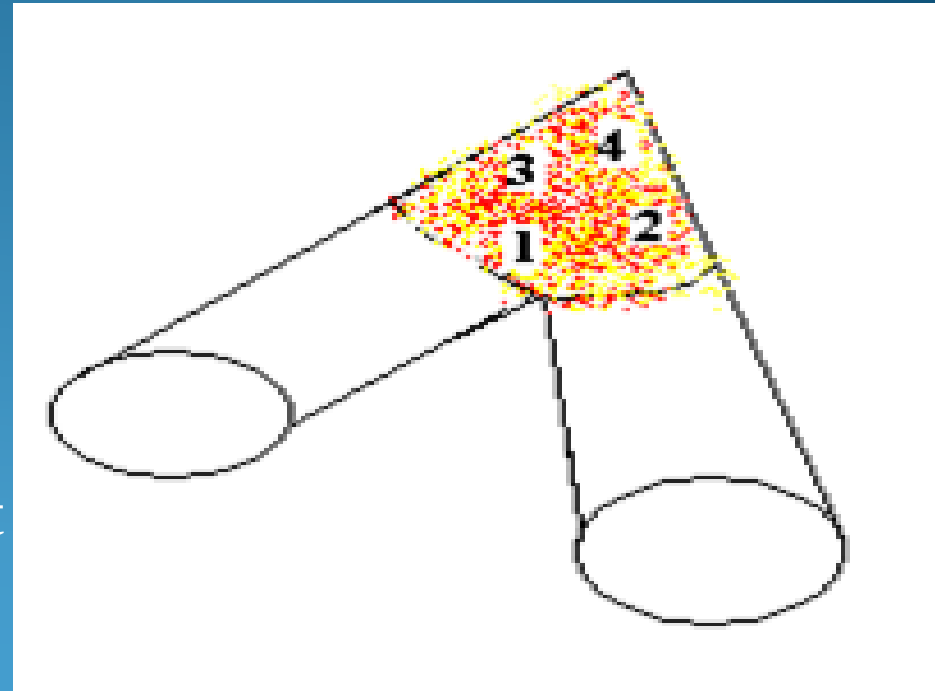


# V-Mixing Module

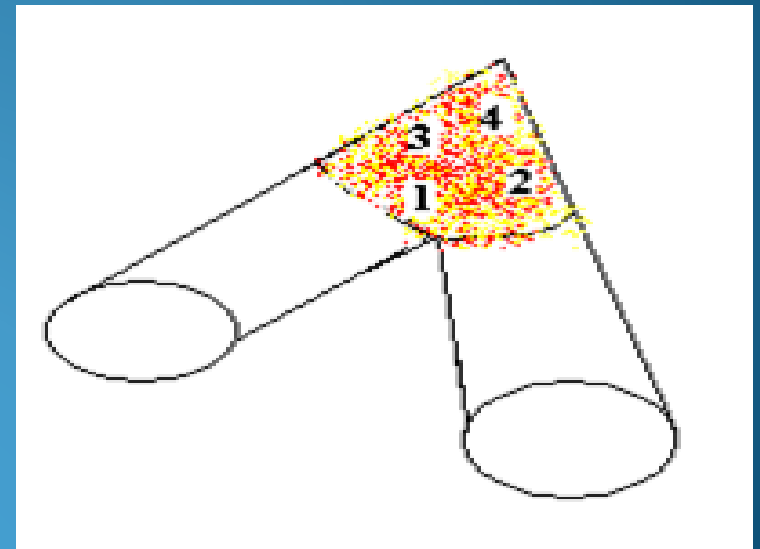
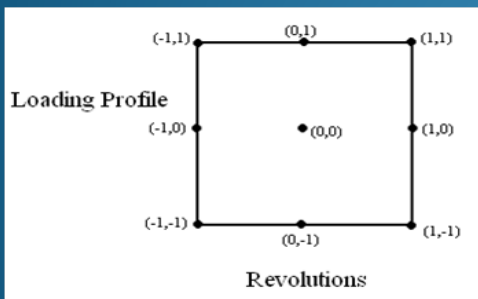
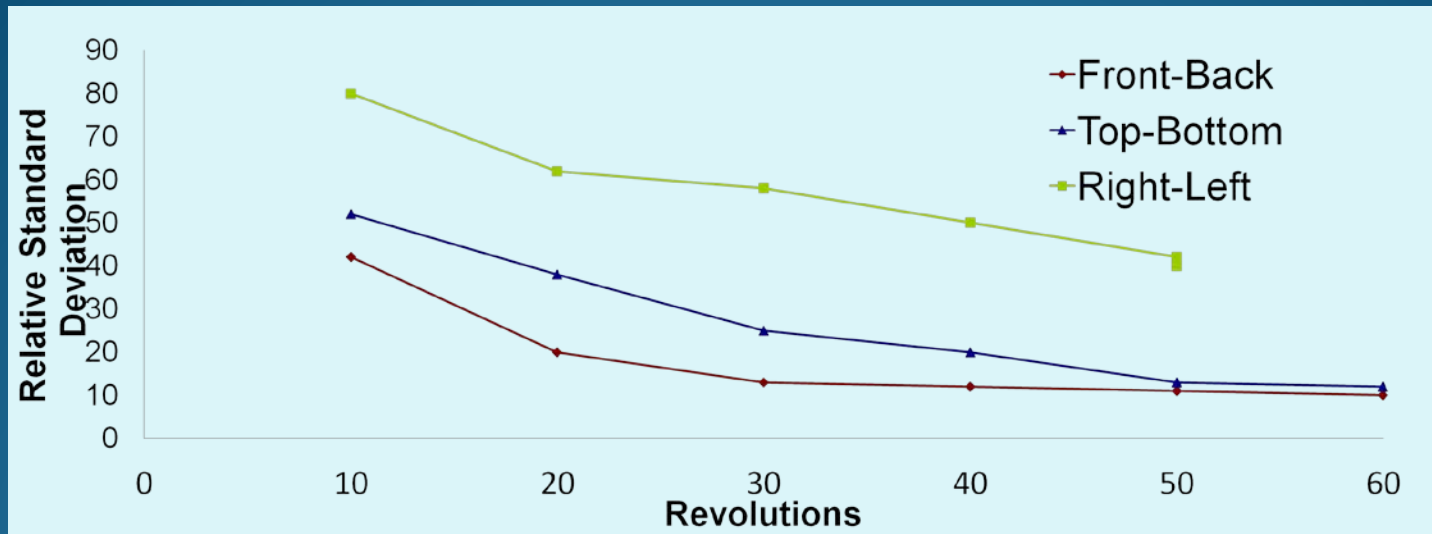
- Introduces students to mixing of solids with pharmaceutical applications
- No constitutive equations
- Introduce students to design of experiments (DOE)
- Students previously exposed to basic statistics and t distribution

# V-Mixer Experiments (colorimetric measurement)

- 90 – 110 micron polyarmor<sup>®</sup> particles
- Red and yellow particles
- Yellow dye soluble in methanol
- Mix, sample, spectrometer measurement  
 $\lambda = 570 \text{ nm}$



# Spectral Colorimetric Measurements - Mixing Quality



Loading Profile		Revolutions	
<i>Coded</i>	<i>Actual</i>	<i>Coded</i>	<i>Actual</i>
1	top-bottom	1	18
0	right-left	0	10.5
-1	front-back	-1	3



# Particle Size Distributions

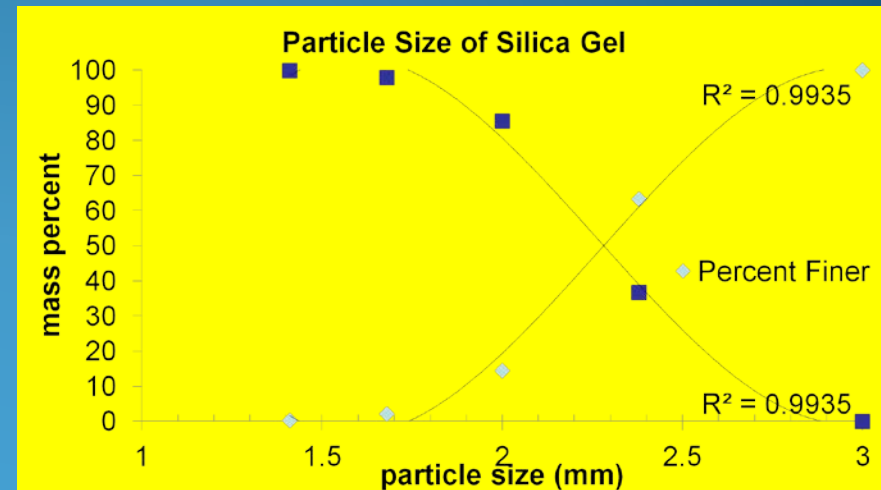
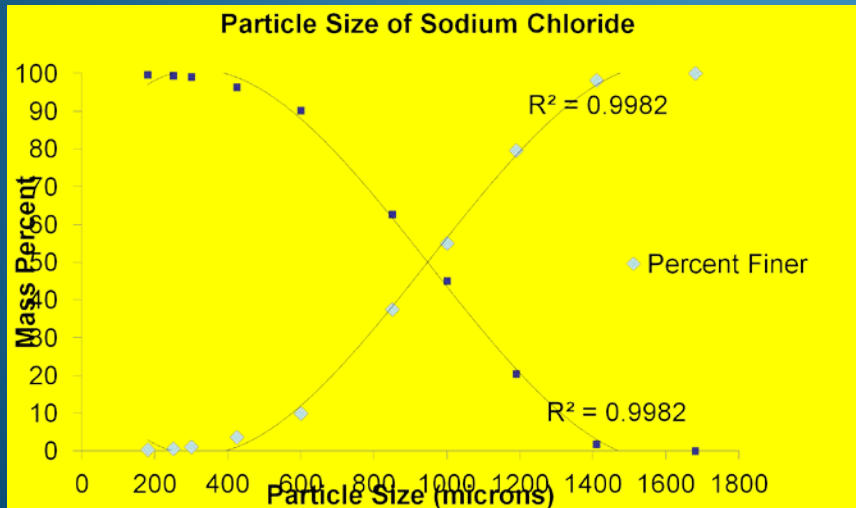
Particle size (shaker method or XCT scan)

Sodium chloride :  $\Phi_{50} = 950 \mu\text{m}$

coefficient of uniformity ( $\Phi_{60}/\Phi_{10}$ ) = 0.67

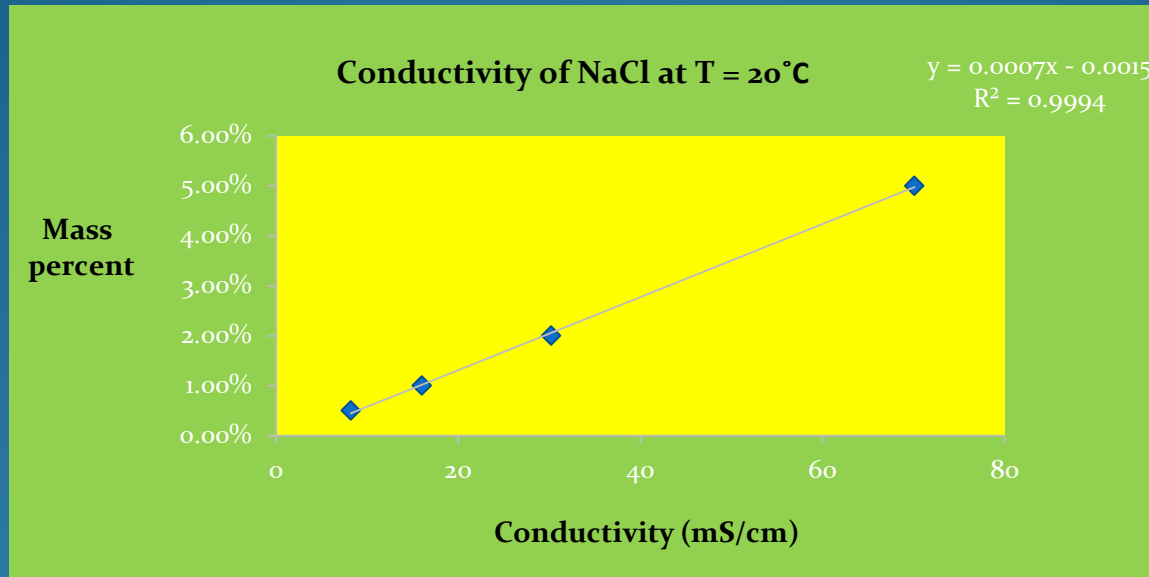
Silica gel:  $\Phi_{50} = 2.27 \text{ mm}$

coefficient of uniformity ( $\Phi_{60}/\Phi_{10}$ ) = 0.82



# Conductivity of NaCl Solution - Quantifies Concentration

## Mixing Quality



Source	Sum of Squares	Df	Mean Square	F-Ratio	P-Value
MAIN EFFECTS					
A:Particle System	10650.2	1	10650.2	148.15	0.0000
B:Loading Profile	559.77	1	559.77	7.79	0.0107
C:Number of Revolutions	609.329	1	609.329	8.48	0.0081
RESIDUAL	1581.53	22	71.8879		
TOTAL (CORRECTED)	13380.7	25			



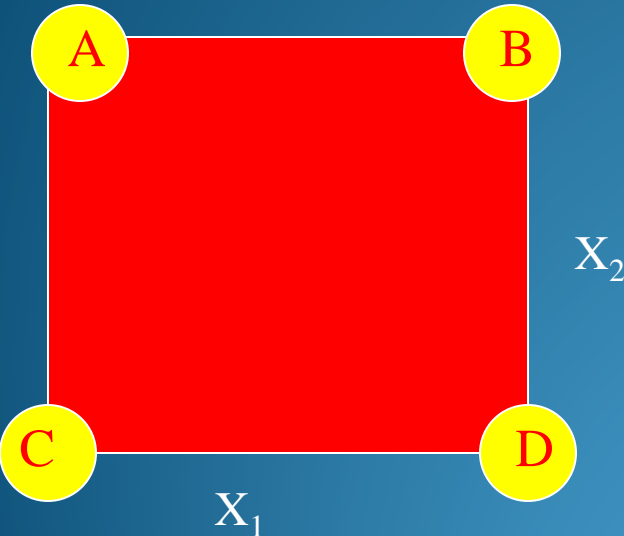
# Let's Experiment!

- Four (4) V-mixers
- Load mixers at design points
- Variables: particle (colored spheres) size and loading profile
- Constant: mixing speed, mixing time, V-mixer fill, sphere size ratio
- Very basic experimental design concepts before forming groups

# V-Mixer Experiment

2 level factorial for two variables

$2^2$  factorial



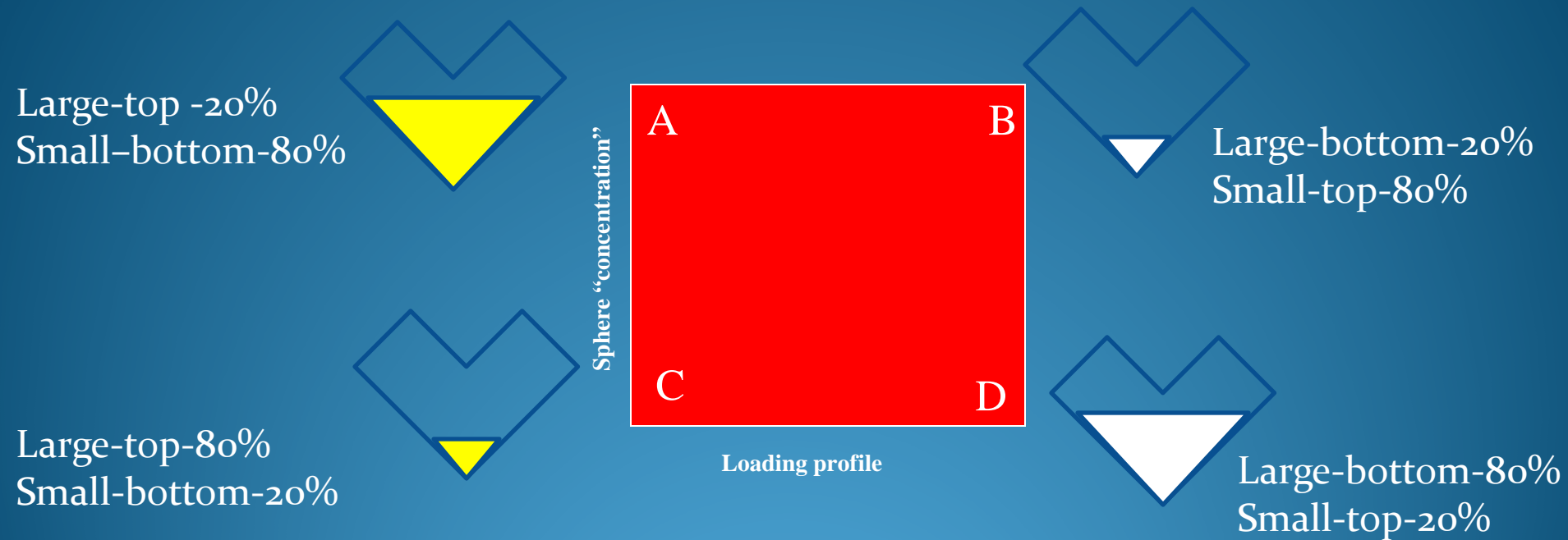
1. Average results at high and low values of  $x_1$  and  $x_2$
2. Compute difference between average result at high and low values of  $x_1$  and  $x_2$
3. Compare difference to MSFE at desired confidence level
4. Do “center point” experiments to test curvature
5. Compare “center point” average to MSCE at desired confidence level

Results:

- Identify statistically significant variables
- Develop algebraic model for measured variable as function of independent variables  $x_1$  and  $x_2$  and their interactions

# V-Mixer Experiment (not to scale)

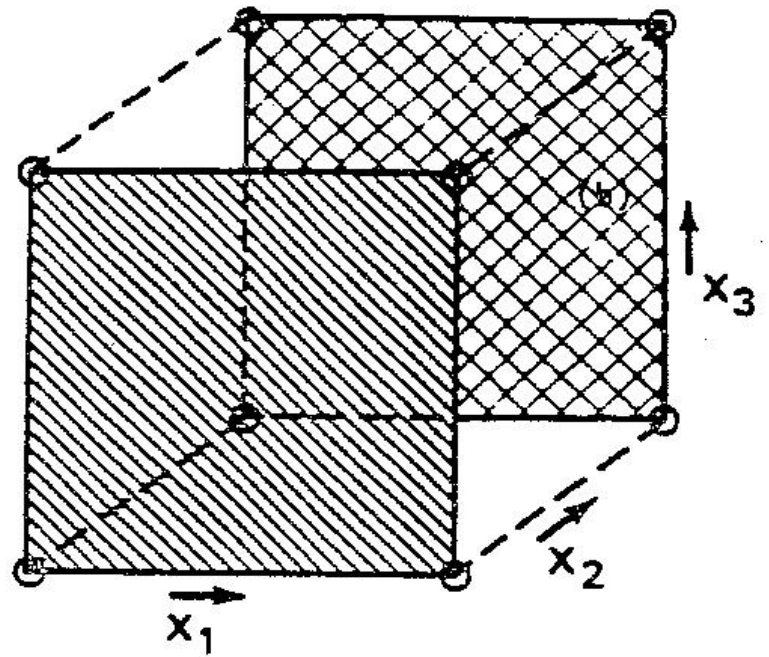
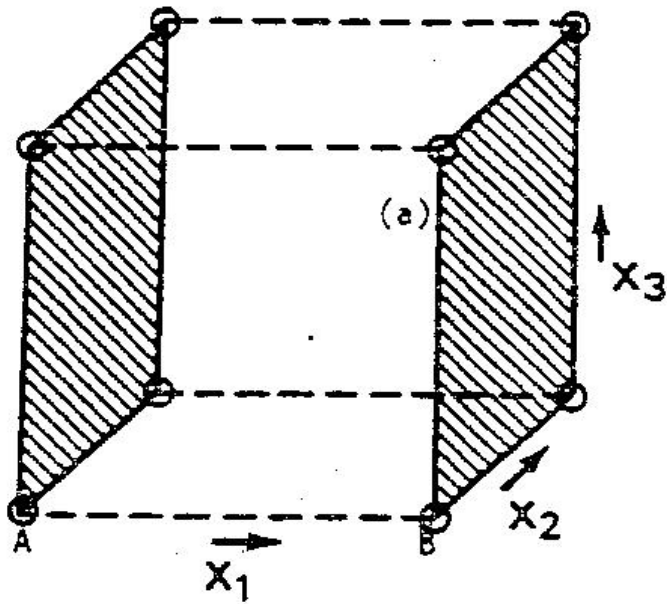
(measurements – weight %)



Spheres - particle size and location in mixer  
constant ratio 80/20  
constant V-mixer fill

large spheres      **small spheres**

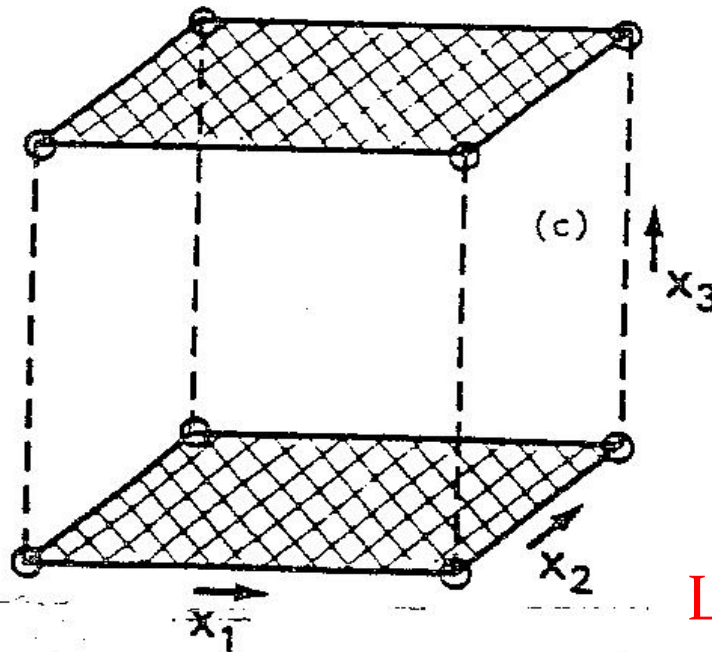




### Experimental design

- Hidden replication- less experiments

- Orthogonality - independence among variables



Let's form groups

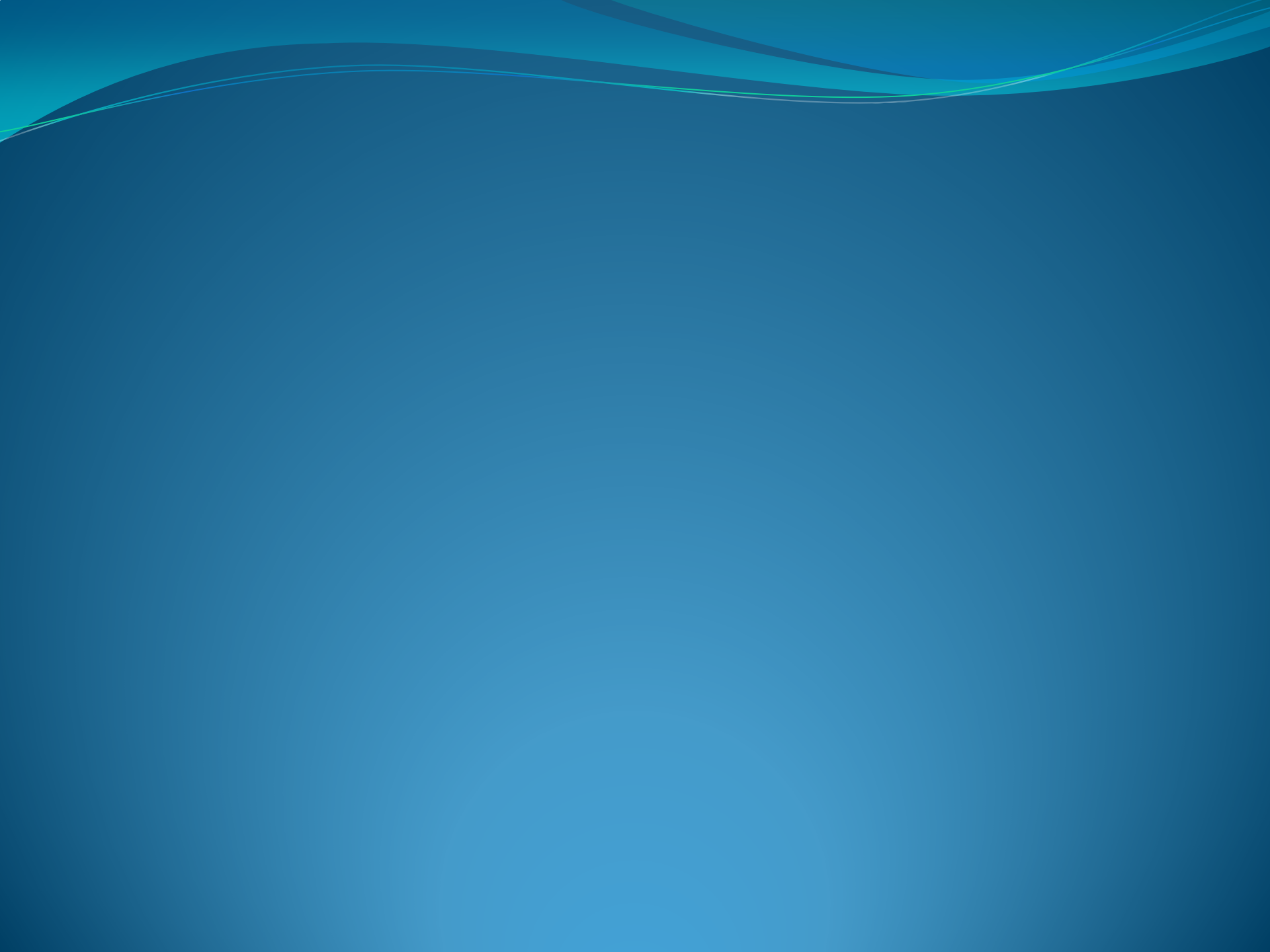


# Acknowledgements

- C. Del Vecchio
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- H. Diallo
- **M. Harris, ChE Technician**



This work is part of a publication in progress.



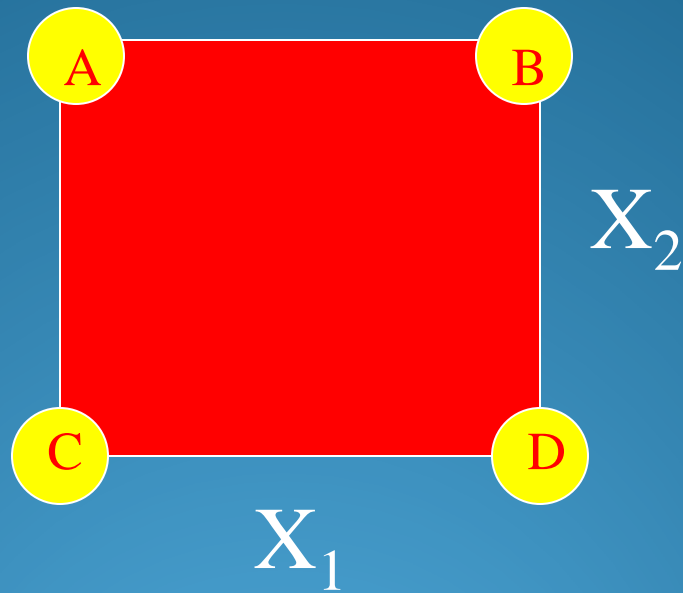
# Number of Experiments: OFAAT v. Design

- Extraction of herbicide from soil matrix
  - quantification of residue and sample preparation
- Variables: solvent, co-solvent, T, P, soil matrix, operation mode
- OFAAT: 3 variable values, 2 modes of operation
  - $N = (3)(3)(3)(3)(3)(2) = 486$
- Factorial design:  $2(2^5) = 64$
- Design: minimum experimental runs, inclusive and accurate analysis

# Properties of Factorial Designs

- Hidden replication
  - all points are used to calculate effect on variables and interactions
- Orthogonal (independent measurements)

# Interactions Independent Variables



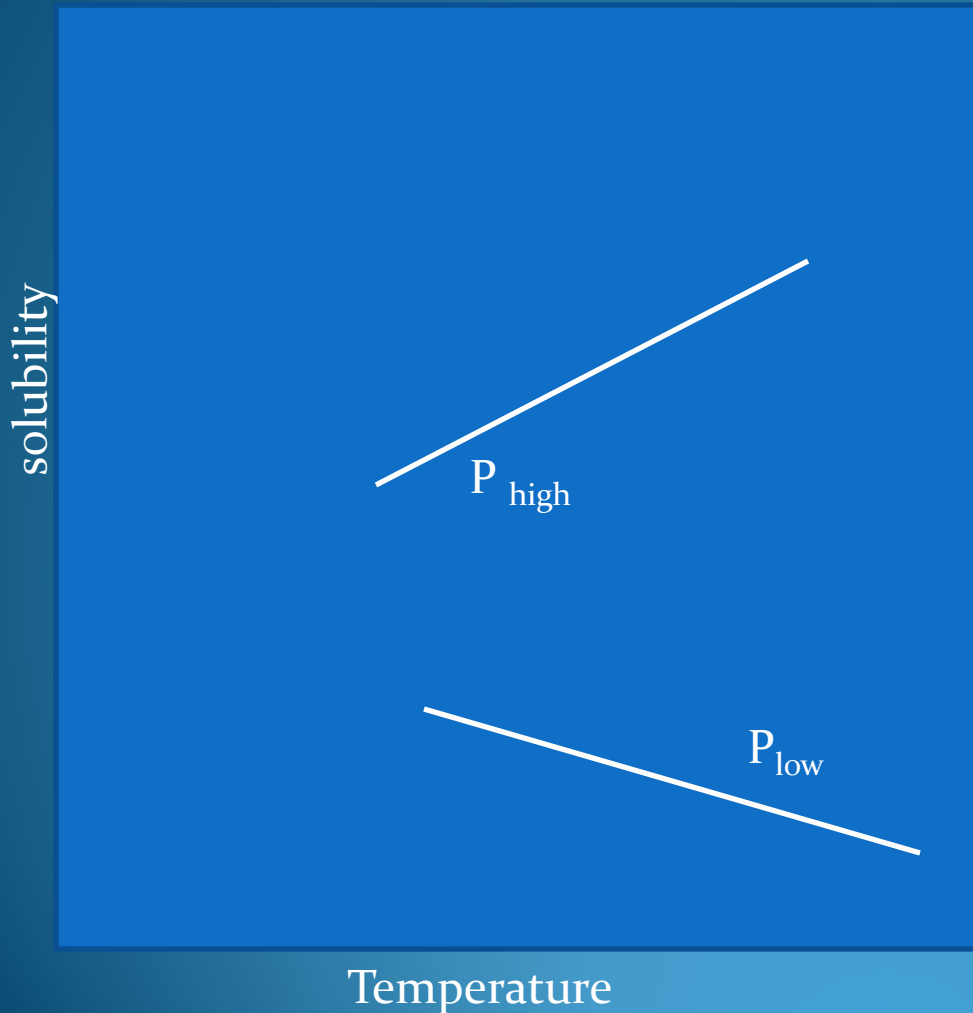
# Interactions Independent Variables

- $I_n = \frac{1}{2} [(b - a) - (d - c)]$
- If more than 2 factors – compare diagonally opposing planes



# Interaction Example

## Solid Solubility in SF CO<sub>2</sub>



Solubility =  $f(\text{CO}_2 \text{ density, solid volatility})$

T $\uparrow$  volatility  $\uparrow$  density  $\downarrow$

P<sub>high</sub> - density high

P<sub>low</sub> - density low

# Design: Coding Factors

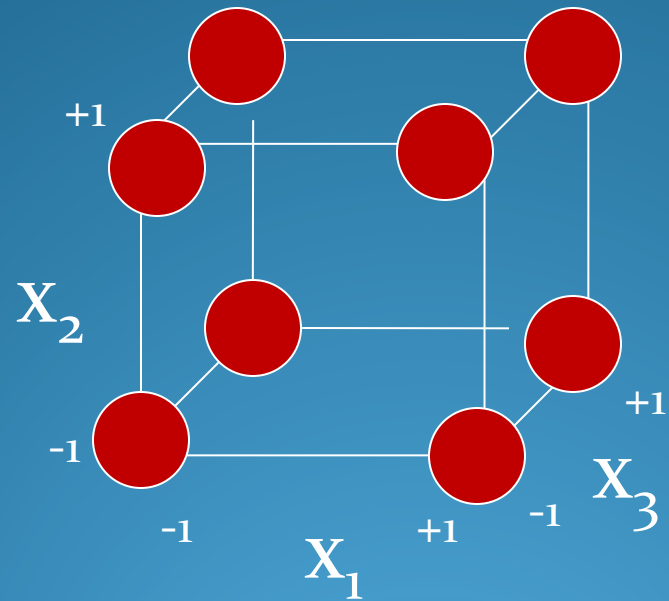
- Code factors for tabular analysis
  - discrete: + and –
  - continuous: high +  
low -
- Interpret + and – as +1 and -1
- Space widely for larger response

Factors

Trial

	$x_1$	$x_2$	$x_3$	$x_4$	$x_5$
1	-	-	-	-	-
2	+	-	-	-	-
3	-	+	-	-	-
4 = $2^2$	+	+	-	-	-
5	-	-	+	-	-
6	+	-	+	-	-
7	-	+	+	-	-
8 = $2^3$	+	+	+	-	-
9	-	-	-	+	-
10	+	-	-	+	-
11	-	+	-	+	-
12	+	+	-	+	-
13	-	-	+	+	-
14	+	-	+	+	-
15	-	+	+	+	-
16 = $2^4$	+	+	+	+	-
17	-	-	-	-	+
18	+	-	-	-	+
19	-	+	-	-	+
20	+	+	-	-	+
21	-	-	+	-	+
22	+	-	+	-	+
23	-	+	+	-	+
24	+	+	+	-	+
25	-	-	-	+	+
26	+	-	-	+	+
27	-	+	-	+	+
28	+	+	-	+	+
29	-	-	+	+	+
30	+	-	+	+	+
31	-	+	+	+	+
32 = $2^5$	+	+	+	+	+

# $2^3$ Factorial Design



## Computational table for a $2^3$ Factorial Design

Run	mean	$X_1$	$X_2$	$X_1 X_2$	$X_3$	$X_1 X_3$	$X_2 X_3$	$X_1 X_2 X_3$	$\bar{Y}$
1	+	-	-	+	-	+	+	-	
2	+	+	-	-	-	-	+	+	
3	+	-	+	-	-	+	-	+	
4	+	+	+	+	-	-	-	-	
5	+	-	-	+	+	-	-	+	
6	+	+	-	-	+	+	-	-	
7	+	-	+	-	+	-	+	-	
8	+	+	+	+	+	+	+	+	
$\Sigma+$ $\Sigma-$ D E	$D = \Sigma+ - \Sigma-$ $E = D/4$								

Y = measured variable, compare E to MSFE, average of center measurements compared  
 To MSCE if abs. value of E > MSFE – significant at confidence level . If center average > MSCE – nonlinearities  
 Significant at confidence level





# Accounting for Curvature

- Non-linear effects
- Run center points ( +1=150 and -1= 50 then center point, 0 = 100)
- Severity of curvature quantified by minimum significant curvature effect

## Factor Effect Significance: Minimum Significant Factor Effect

- $MSFE = t \cdot s(2/mk)^{1/2}$

t= student's t at desired confidence level  
and appropriate degrees of freedom

s= standard deviation

m = number of + signs in column

k= number of replicates



## Curvature Effects: Minimum Significant Curvature Effect

- $$\text{MSCE} = t \cdot s \left[ \frac{1}{mk} + \frac{1}{c} \right]^{1/2}$$

all variables as defined and  $c =$  number of center points

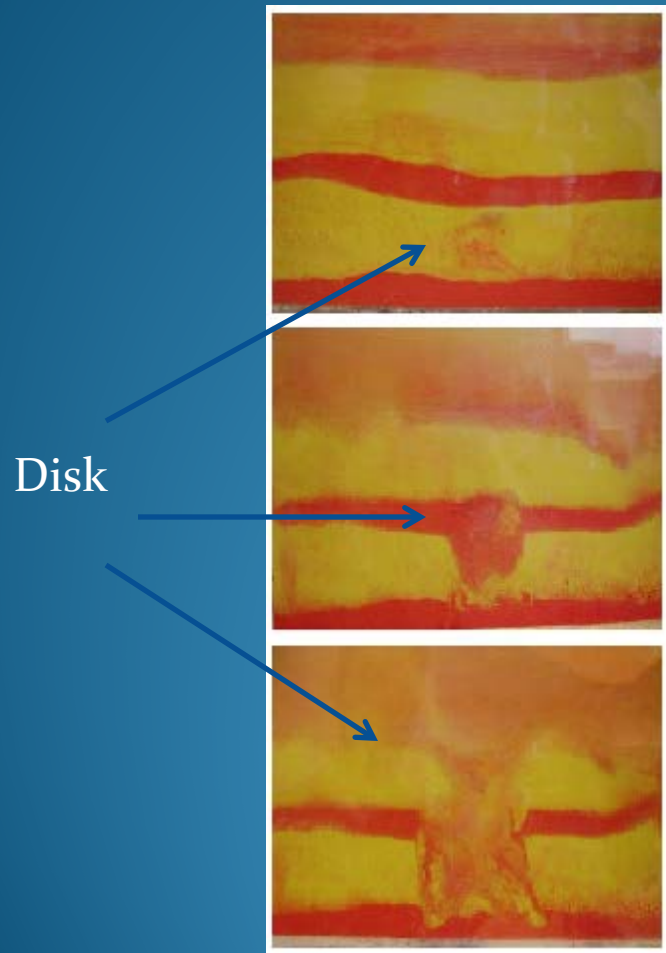
# Coding and Model from Experimental Data

- Code  $X(\text{coded}) = \frac{X - (\text{high} + \text{low})/2}{(\text{high} - \text{low})/2}$

$X$  = the value of the independent variable at which a prediction is desired



# Large Particle Rise in Smaller Particle Bed



8	6-32 thread 7/64 hex head screws
2	10" by 10" acrylic plastic sheets
4	10" by 1" acrylic plastic sheets
1	10" by 1" gasket

- 2-D square vessel (10")
- Sealed
- Flat metal disc  $d = 1"$